

Hydrogen Recycle in a Refinery.

Hydrogen is a critical commodity in a petroleum refinery. Alvar and Towler (2002) describe a case study involving the optimization of a hydrogen distribution system within a refinery, and it is comprised of four sinks and six sources. The pertinent information regarding these sinks and sources is given in Tables 1 and 2.

In this case study, fresh hydrogen is available with a 5% mol/mol impurity content. Identify the target for minimum usage of fresh hydrogen and minimum discharge of gaseous waste.

Table 1. Sink data for hydrogen problem (Alvar & Towler 2002)

| Sinks | Flow (mol/s) | Maximum Inlet Impurity Concentration mol-% | Load (mol/s) |
|-------|--------------|--|------------------------|
| 1 | 2495 | 19.39 | 483.8 483.8 |
| 2 | 180.2 | 21.15 | 38.1 |
| 3 | 554.4 | 22.43 | 124.4 |
| 4 | 720.7 | 24.86 | 179.2 |

Table 2: Source data for the hydrogen problem

| Sources | Flow mol/s | Impurity conc mol-% | Load (mol/s) |
|---------|------------|---------------------|--------------|
| 1 | 623.8 | 7 | 43.7 |
| 2 | 415.8 | 20 | 83.2 |
| 3 | 1801.9 | 25 | 450.5 |
| 4 | 138.6 | 28 | 34.7 |
| 5 | 346.5 | 27 | 93.6 |
| 6 | 457.4 | 30 | 137.2 |

Sink data
Flow
mol/s
2495

Load
mol/s
483.8

$$2495 + 180.2 = 2675.2$$

$$2675.2 + 554.4 = 3229.6$$

$$3229.6 + 720.7 = 3950.3$$

$$483.8 + 38.1 = 521.9$$

$$521.9 + 124.4 = 646.3$$

$$646.3 + 179.2 = 825.5$$

Source data.

Flow (mol/s)
623.8

Load (mol/s)
43.7

$$623.8 + 415.8 = 1039.6$$

$$1039.6 + 1801.9 = 2841.5$$

$$2841.5 + 138.6 = 2980.1$$

$$2980.1 + 346.5 = 3326.6$$

$$3326.6 + 457.4 = 3784$$

$$43.7 + 88.2 = 126.9$$

$$126.9 + 450.5 = 577.4$$

$$577.4 + 34.7 = 612.1$$

$$612.1 + 93.6 = 705.7$$

$$705.7 + 137.2 = 842.9$$

